



Microscale Enhancement of Heat and Mass Transfer for Hydrogen Energy Storage

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Oregon State University

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Hydrogen Storage Engineering

CENTER OF EXCELLENCE

ST 046

This presentation does not contain any proprietary, confidential, or otherwise restricted information



Overview

Timeline

- Feb 1st 2009 start
- Jan 31st, 2014 finish
- 8% Complete

Budget

- Total project funding
 - DOE - \$2,398,935
 - Contractor - \$600,345
- Funding received in FY09 - \$300,00
- Funding for FY10 - \$350,000

Barriers

- Barriers addressed
 - A) System Weight and Volume
 - E) Charging and Discharging Rates
 - H) Balance of Plant

Partners

- **HSECoE Partners** - SNRL, PNNL, LANL, NREL, JPL, United Technologies, TRC, GM, Ford, BASF, Lincoln Composite, HSM, UQTR
- **Center Lead** - SNRL



Hydrogen Storage Engineering Center of Excellence

D. Anton, SRNL
T. Motyka, SRNL

Materials Operating Requirements

D. Herling, PNNL

- Materials Centers of Excellence Collaboration – SRNL, LANL, NREL
- Reactivity – UTRC
- Adsorption Properties – UQTR
- Metal Hydride Properties – SRNL
- Chemical Hydride Properties - LANL

Transport Phenomena

B. Hardy, SRNL

- Bulk Materials Handling – PNNL
- Mass Transport – SRNL
- *Thermal Transport – SRNL, OSU*
- Media Structure - GM

Enabling Technologies

J. Reiter, JPL

- Thermal Insulation – JPL
- Hydrogen Purity – UTRC
- Sensors – LANL
- Materials Compatibility – PNNL
- Pressure Vessels – PNNL
- *Thermal Devices - OSU*

Performance Analysis

M. Thornton

- Vehicle Requirements – NREL
- Tank-to-Wheels Analysis – NREL
- Forecourt Requirements - UTRC
- Manufacturing & Cost Analysis - PNNL

Integrated Power Plant/ Storage System Modeling

D. Mosher, UTRC

- Off-Board Rechargeable - UTRC
- On-Board Rechargeable – GM
- Power Plant – Ford

Subscale Prototype Construction, Testing & Evaluation

T. Semelsberger, LANL

- Risk Assessment & Mitigation – UTRC
- System Design Concepts and Integration - LANL
- Design Optimization & Subscale Systems – LANL, SRNL, UQTR
- Fabricate Subscale Systems Components – SRNL, LANL
- Assemble & Evaluate subscale Systems – LANL, JPL, UQTR

Technology Area

Technology Area Lead

- Technology Team – TT Lead
- Technology Team – TT Lead
- Technology Team – TT Lead

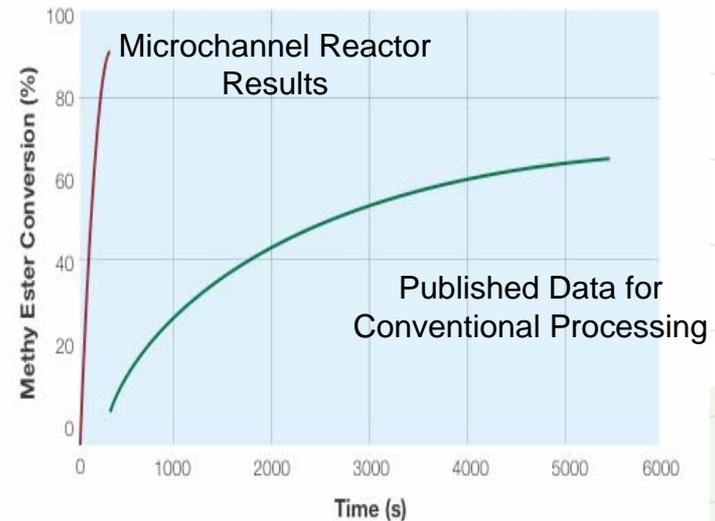
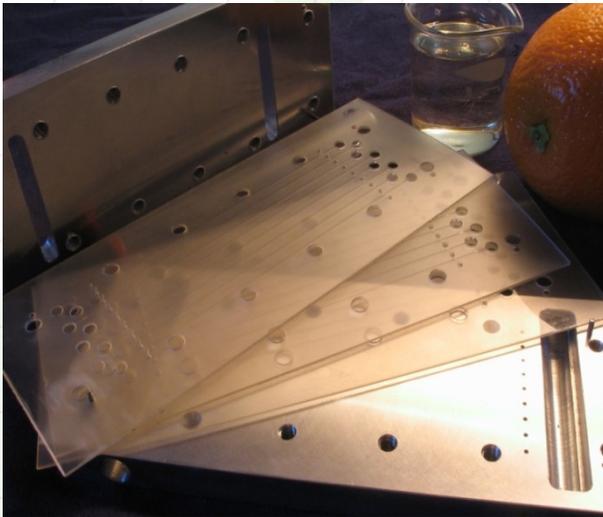


Relevance -Objectives

- **Objective** – Use microchannel technology to ...
 - 1) reduce the size and weight of storage,
 - 2) improve charging and discharging rate of storage
 - 3) reduce size and weight and increase performance of thermal balance of plant components.
- **Barriers Addressed**
 - Reduce system size and weight (Barrier A)
 - Charging and Discharging rates (Barrier E)
 - Balance of Plant (Barrier H)

Relevance – What are microtechnology-based Energy and Chemical Systems (MECS)?

- MECS uses microscale dimensions in flow paths (microchannels) to enhance heat and mass transfer
- For processes limited by diffusion, laminar flow residence time (and to some extent size) decreases as D^2 where D is channel width. **In many energy and chemical systems, diffusion is the limiting phenomena. The use of microchannels addresses this barrier**





Relevance – MECS Features and Hydrogen Storage

- Significant reduction in size and weight when a process is limited by diffusion
 - **Reduces storage size and weight related to heat and mass transfer**
 - **Reduces size of balance of plant thermal components**
 - **Reduces charging time**
- High degree of control over process
 - **Optimizes storage for weight minimization**
- Number up rather than scale up
 - **Maintain optimum performance attained in a single unit cell**
- Complexity can be added without increasing cost
 - **Integrate hydrogen distribution in cooling surfaces**
- Low thermal mass and high heat and mass fluxes will allow rapid start-up and response to transients
- In the temperature range of interest, attractive high volume manufacturing options exist.



Approach - Programmatic

- **Phase 1: System Requirements & Novel Concepts**
 - OSU will focus on simulation and experimental investigations to identify and prioritize opportunities for applying microscale heat and mass transfer enhancement techniques.
 - Working with other team members, OSU will identify the highest value applications and conduct experimental investigations and modeling to collect data necessary to support the Go/No-Go decision to proceed to Phase 2.
- **Phase 2: Novel Concepts Modeling, Design, and Evaluation**
 - For each high-priority application, OSU will develop predictive models, design and evaluate components, fabricate proof-of-principle test articles, conduct proof-of-principle tests, and use the results to validate the predictive models.
 - With other team members, OSU will select one or more high-priority components for prototype demonstration.
- **Phase 3: Subsystem Prototype Construction, Testing, and Evaluation**
 - For each high-priority component, OSU will design, optimize, and fabricate the component.



Approach – Phase One Technical Approach

- For each high priority component, use microchannel technology to reduce barriers to heat and mass transfer.
- Optimize the performance of a single unit cell (i.e. an individual microchannel) and then “Number Up”
 - Develop appropriate simulation tools
 - Validated simulation tools by experimental investigations
 - Use simulation to optimize a unit cell
- Explore microlamination as a path to “numbering up” by low cost high volume manufacturing (see Supplemental Slides).



Approach – Milestones and Go/No Go Decision Criteria

- **2009/2010 Milestones**
 - Complete identification of the highest value applications of microchannel-based technology (2/1/2010).
 - Complete experimental investigations and modeling to collect data that will support the Go/No-Go decision to proceed to Phase 2 (3/1/2011).
- **Phase I Go/No Go Criteria**
 - Identify and demonstrate, through experiment and simulation, one or more high priority applications where the application of microchannel technology can make a significant contribution to meeting DOE 2015 performance goals
 - Develop specific performance, weight and size goals for each application included in the OSU phase 2 scope of work.
- **Phase II Go/No Go Criteria**
 - Complete successful proof of principle tests for high priority microchannel applications identified in Phase 1 and demonstrate that based, on the proof-of-principle tests, a prototype microchannel component can meet the DOE 2015 goals.



Technical Accomplishments

- **Technical Progress Relative to 2009/2010 Milestones** - Completed identification of highest value applications:
 - 1) MECS-based Tank Insert
 - 2) MECS-based Integrated Hydrogen Combustor and Heat Exchanger
- **Technical Progress relative to Objectives:**
 - 1) Reduce the size and weight of storage – **MECS-based Tank Insert Development**
 - 2) Improve charging and discharging rate of storage – **MECS-based Tank Insert Development**
 - 3) Reduce size and weight and increase performance of thermal balance of plant components – **MECS-based integrated combustor/heat exchanger**



Accomplishments (Barriers A and E) - MECS-based Tank Insert

- MECS-based Tank Insert Concept
 - Use microchannels to both cool and distribute H_2 in a plate with a thickness < 1 mm.
 - A unit cell will consist of two liquid cooled plates separated by metal hydride
 - The tank insert will consist of multiple unit cells with headers for cooling fluid and hydrogen distribution

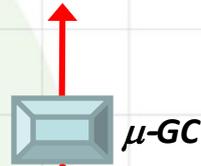
Accomplishments (Barriers A and E) - Tank Insert Unit Cell Testing



Experimental Data Collection

- Temperature
- Pressure
- Displacement of compression spring
- Gas Composition

Top and bottom plates can be removed to allow easy access to reaction vessel.



H_2 Exit

Spring to provide constant force acting on hydride powder and equipped with strain gage

Metal hydride powder will be patterned with micro-channels to investigate effect on H_2 gas distribution throughout reaction volume

Pressurized N_2 in void space

Integrated hydrogen distribution plate and heat exchanger

High pressure outer shell

Glass filled PTFE reaction vessel

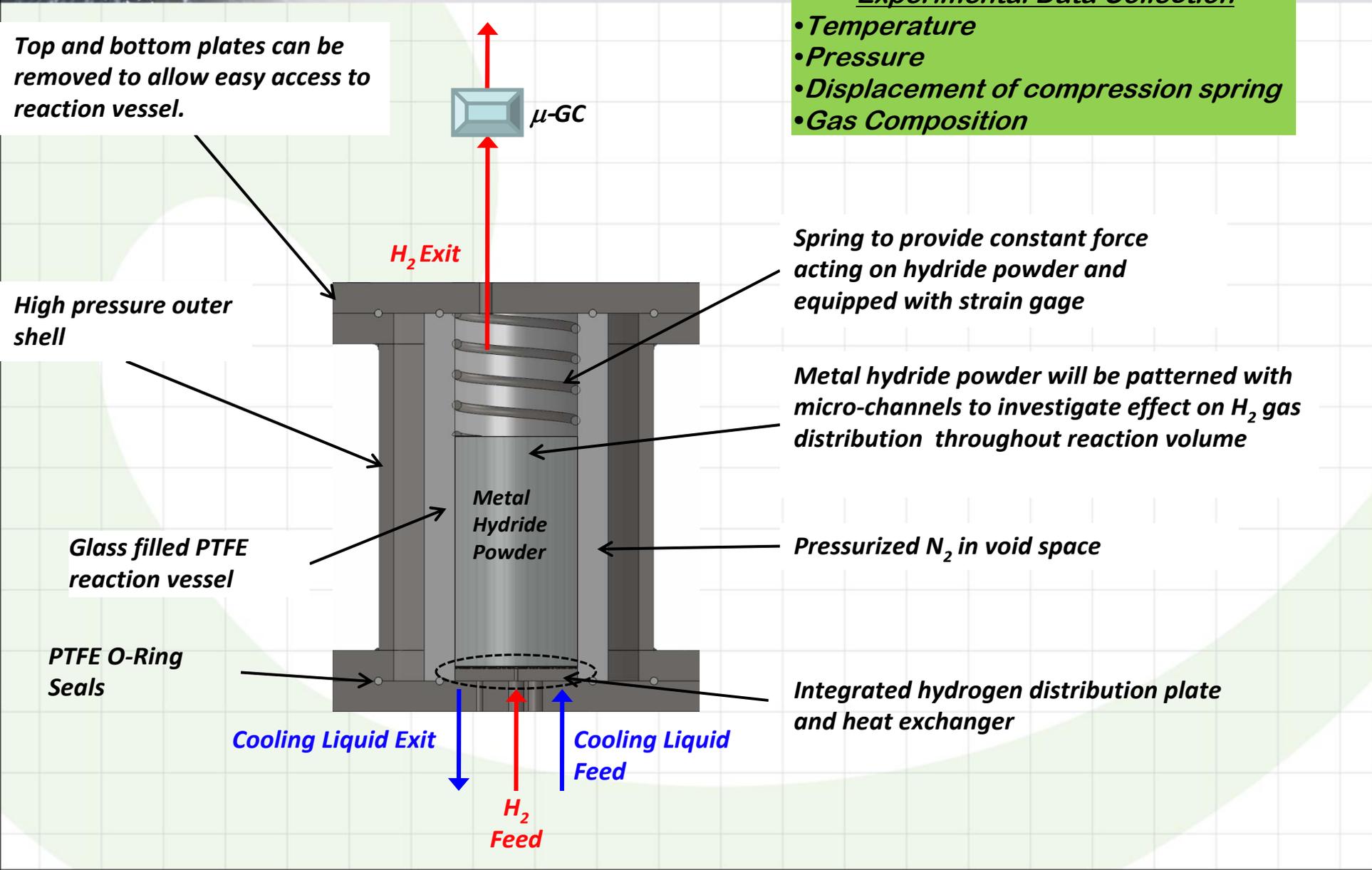
Metal Hydride Powder

PTFE O-Ring Seals

Cooling Liquid Exit

H_2 Feed

Cooling Liquid Feed

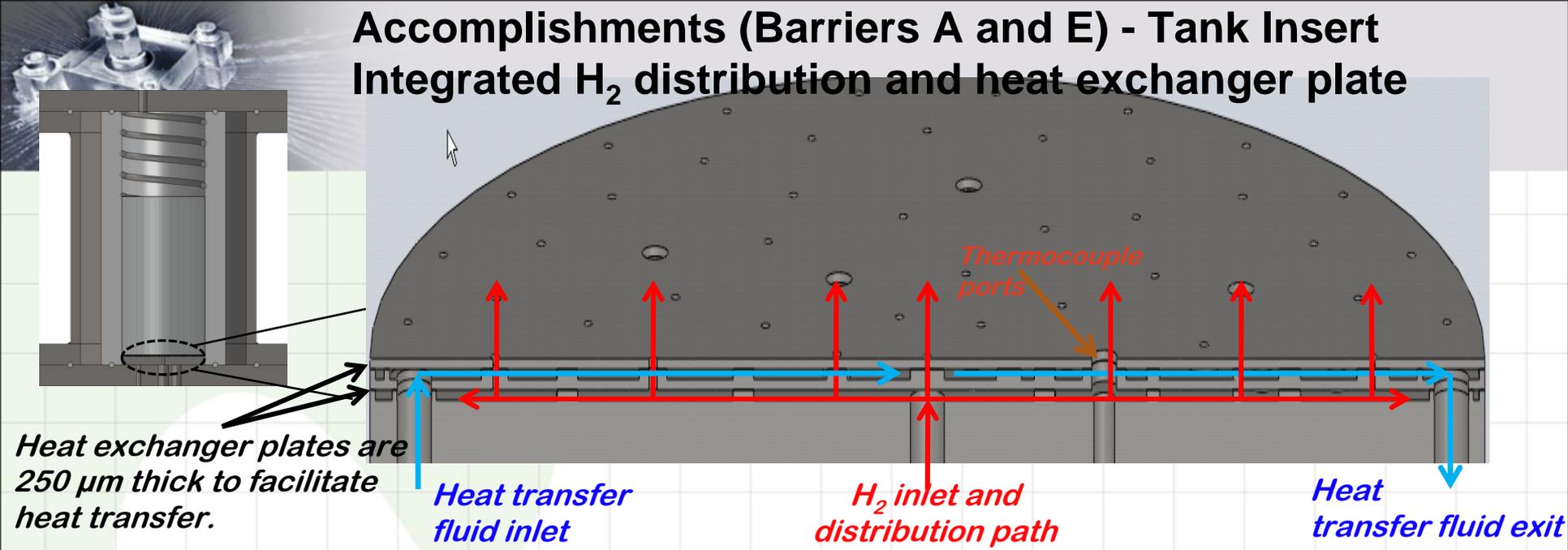




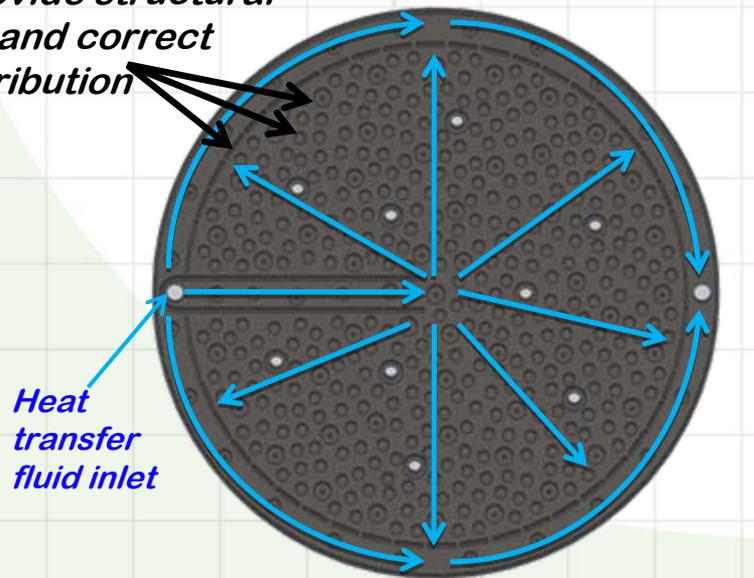
Accomplishments (Barriers A and E) - Tank Insert Unit Cell Testing



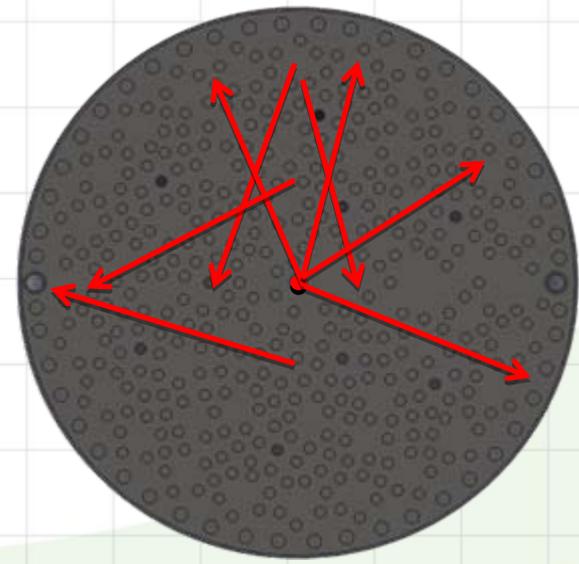
Accomplishments (Barriers A and E) - Tank Insert Integrated H₂ distribution and heat exchanger plate



Pillars and wall features are 250 μm tall to provide structural integrity and correct fluid distribution



Top view of heat exchanger plate



Top view of H₂ distributor plate – H₂ inlet in center; distributes evenly; exits through holes in next layer



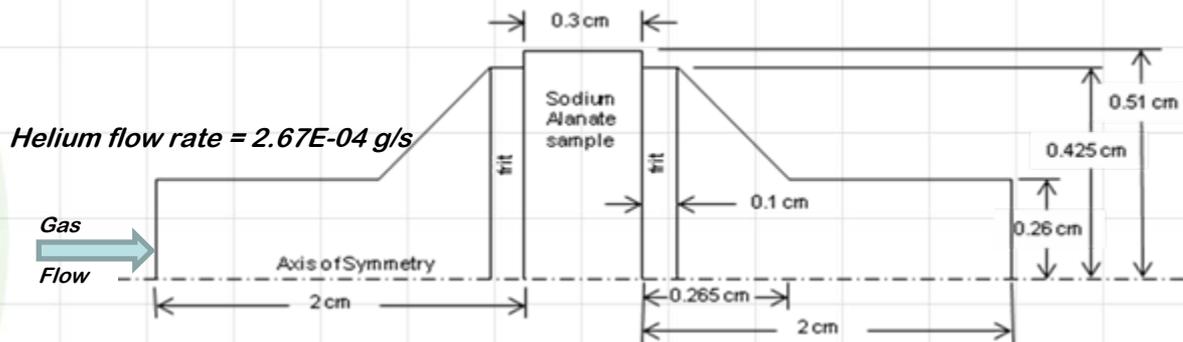
Accomplishments (Barriers A and E) – Modeling & Simulation

- Full multiphase Navier-Stokes equations solved, accounts for mass and energy transport between gas and hydride phases
- Non-reacting gas pressure drop validated against SNL data (Dedrick et al, 2009)
- Two-step reaction kinetics as a function of temperature, pressure, and concentration validated against UTRC and SRNL data
- Tank models indicate that external combustors are sufficient for full discharge



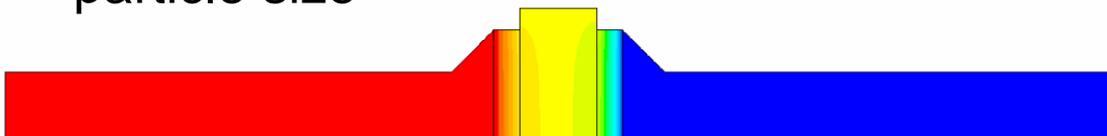
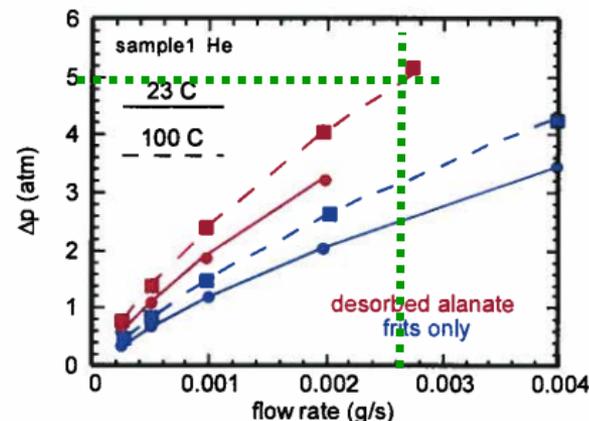
Accomplishments (Barriers A and E) – Model Validation

- The graph below shows pressure drop through the experimental device published by Dedrick et al (2009)



Geometry used in the pressure drop validation study (Dedrick et al)

- Total pressure drop through the device with alanate present is shown by red lines
- Our predicted pressure drop (- - -) correlates well with the experimental data
- Model results are extremely sensitive to particle size



Contours of pressure drop through the model of the test device using particle diameters of 1.5 and 2 microns in the alanate and frit, respectively.



Accomplishments (Barriers A and E) - Tank Insert Development

TASKS/Months	Nov-09	Dec-09	Jan-10	Feb-10	Mar-10	Apr-10	May-10	Jun-10	Jul-10	Aug-10	Sep-10	Oct-10
Identification of Priority Applications for the Program	■		■	■	■	■	■	■	■	■	■	■
OPTIMIZATION OF THE UNIT CELL OF METAL-HYDRIDE BED												
Conceptual Design	■	■										
Design for Fabrication		■	■	■	■	■						
Safety Review			■	■	■	■						
Fabrication of the Experimental Unit			■	■	■	■	■	■	■	■	■	■
Modelling and Numerical Simulation			■	■	■	■	■	■	■	■	■	■
Experimental Program							■	■	■	■	■	■
Deliverables		1	2	3	4		5					6 7

OPTIMIZATION OF THE UNIT CELL OF ADSORBENT BED												
Conceptual Design					■	■	■					
Design for Fabrication							■	■	■	■	■	■
Safety Review												
Fabrication of the Experimental Unit									■	■	■	■
Modelling and Numerical Simulation												
Experimental Program												
Deliverables												

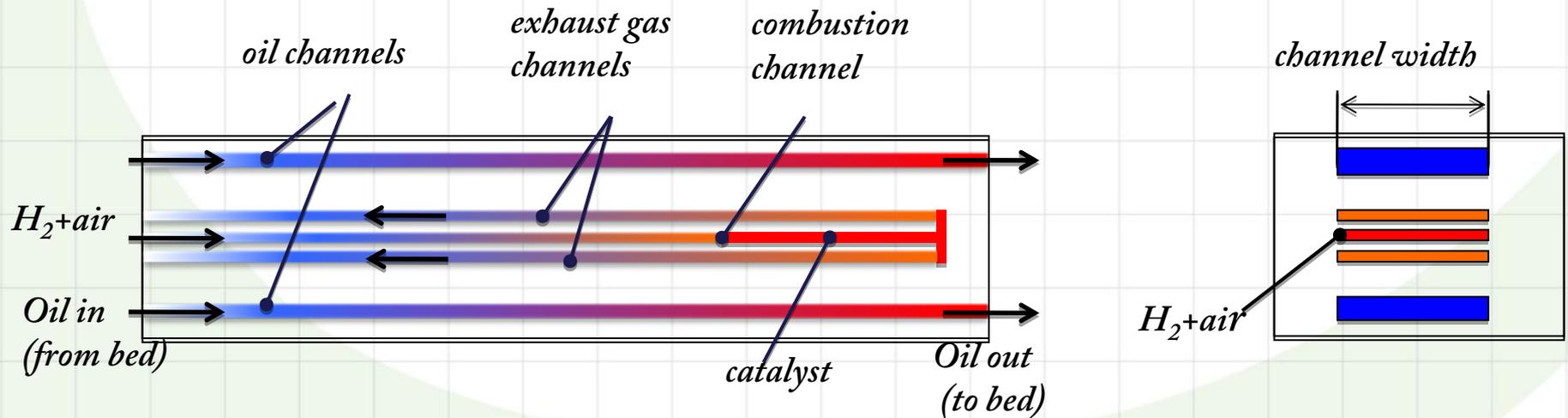
DEFINITION OF DELIVERABLES
1 - Functional Design
2 - Design for Fabrication
3 - Safety Review
4 - Design Modified for Safety
5 - Mathematical Model and Numerical Simulation
6 - Experimental Verification of the Model
7 - Optimized Model Simulation

■	Task current
■	Task accomplished
■	Task in planning stage



Accomplishments (Barrier H) - MECS-based integrated combustor/heat exchanger (μ CHX)

- **Purpose:** Used to heat oil that is used to discharge hydrogen from the hydride bed
- **Relevance:** 90% on-board efficiency calls for a high effectiveness combustion system. Between 8-14 kW energy at around 450 K needs to be supplied to the hydride bed for the discharge cycle
- **Concept:** a microscale device consisting of a combustor, recuperator and oil heat exchanger.
- **Phase I tasks:** Modeling and validation experiments on a small-scale combustor





Accomplishments (Barrier H) - μ CHX Modeling

Approach

- *Mass, momentum, species mass and energy balance*
- *Detailed surface reactions*
- *2-D CFD modeling (Fluent+CHEMKIN-CFD)*
- *Mesh generation in GAMBIT*
- *Minimize use of expensive catalyst*

Status

Preliminary modeling for combustor with surface reactions is ongoing

Adsorption Reactions

1. $\text{H}_2 + \text{Pt(s)} \rightarrow 2\text{H(s)}$
2. $\text{H} + \text{Pt(s)} \rightarrow \text{H(s)}$
3. $\text{O}_2 + 2\text{Pt(s)} \rightarrow 2\text{O(s)}$
4. $\text{O} + \text{Pt(s)} \rightarrow \text{O(s)}$
5. $\text{H}_2\text{O} + \text{Pt(s)} \rightarrow \text{H}_2\text{O(s)}$
6. $\text{OH} + \text{Pt(s)} \rightarrow \text{OH(s)}$

Surface Reactions

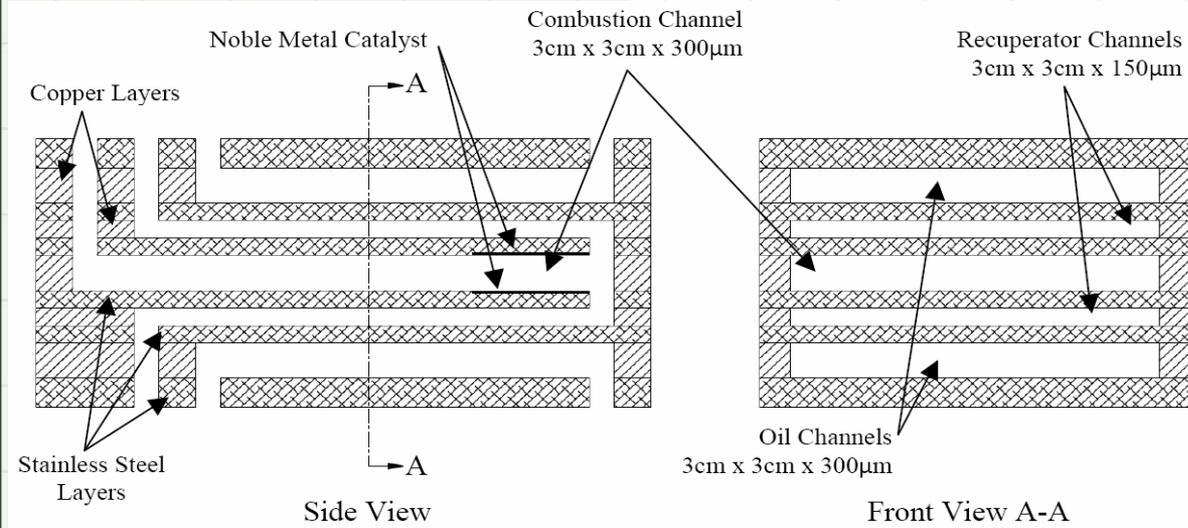
7. $\text{H(s)} + \text{O(s)} \rightarrow \text{OH(s)} + \text{Pt(s)}$
8. $\text{OH(s)} + \text{Pt(s)} \rightarrow \text{H(s)} + \text{O(s)}$
9. $\text{H(s)} + \text{OH(s)} \rightarrow \text{H}_2\text{O(s)} + \text{Pt(s)}$
10. $\text{H}_2\text{O(s)} + \text{Pt(s)} \rightarrow \text{H(s)} + \text{OH(s)}$
11. $\text{OH(s)} + \text{OH(s)} \rightarrow \text{H}_2\text{O(s)} + \text{O(s)}$
12. $\text{H}_2\text{O(s)} + \text{O(s)} \rightarrow \text{OH(s)} + \text{OH(s)}$

Desorption Reactions

13. $2\text{H(s)} \rightarrow \text{H}_2 + 2\text{Pt(s)}$
14. $2\text{O(s)} \rightarrow \text{O}_2 + 2\text{Pt(s)}$
15. $\text{H}_2\text{O(s)} \rightarrow \text{H}_2\text{O} + \text{Pt(s)}$
16. $\text{OH(s)} \rightarrow \text{OH} + \text{Pt(s)}$



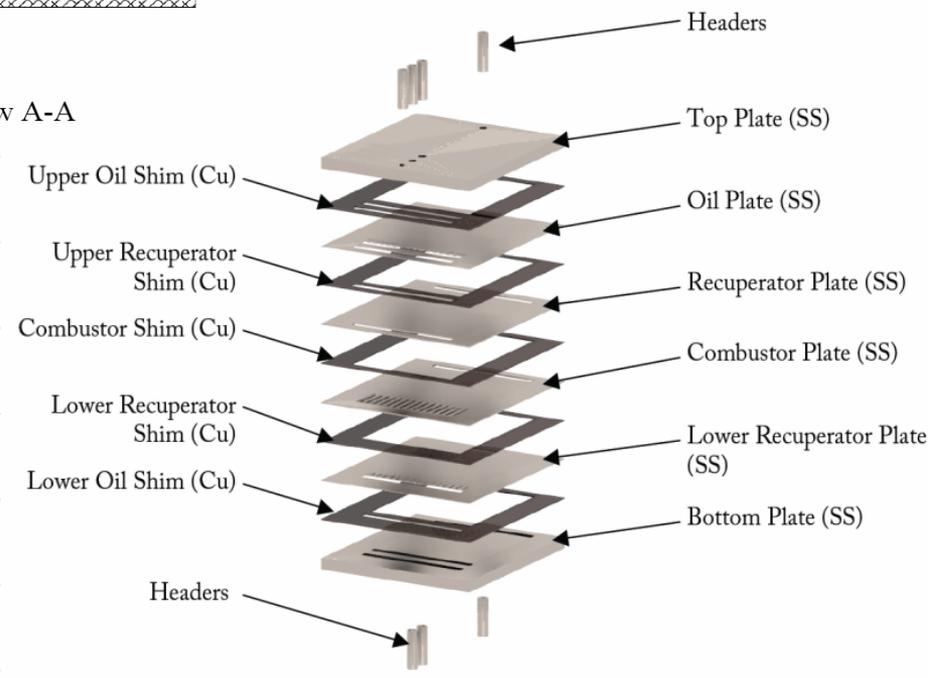
Accomplishments (Barrier H) - μ CHX Unit Cell Testing



Sectional view of Unit Cell test section

Status

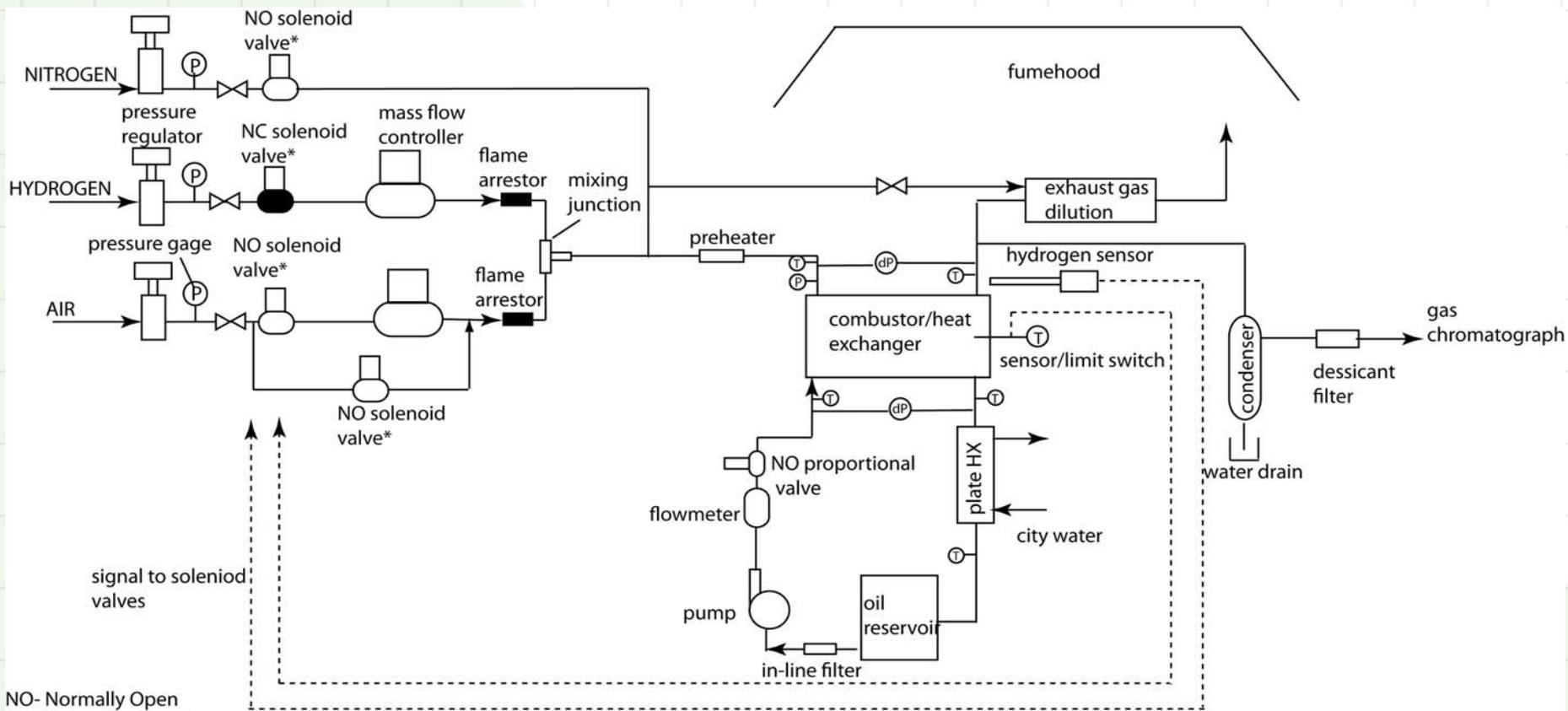
- Preliminary μ -CHX unit cell design completed
- Instrumentation and equipment selected for experimental facility
- Experimental procedure developed
- Safety plan developed to address failure modes for experimental facility



Exploded view of the test section



Accomplishments (Barrier H)- μ CHX Experimental Facility



NO- Normally Open
NC- Normally Closed

* to be controlled by a emergency shutdown button

Mass flow controllers, proportional valve are to be controlled via a LabVIEW program

Pressures , temperatures and flow rates are to be read using a data acquisition unit via a LabVIEW program

Temperature and sensors for safety will be connected independent of the computer



Accomplishments (Barrier H) – Light Weight Microchannel Combustion system for Metal Hydrides

Background : General Motors approached OSU to discuss the possibility of a light weight combustion heating system for desorption of hydrogen from metal hydrides. OSU performed a preliminary conceptual design study and a more detailed CFD analysis in support of this idea. The results suggest that the approach is technically feasible.

Advantages:

- ❖ Eliminates cost and weight (10 to 15 kg) of a number of component in a conventional system
- ❖ faster transient response
- ❖ May increase effectiveness for combustion/heat transfer to hydride

Issues:

- ❖ Small increase in tank weight and volume ($\sim 4500 \text{ cm}^3$)
- ❖ One configuration has safety issues that need to be resolved
- ❖ Joint Intellectual property is being protected



Accomplishments (Barrier H) - Other identified MECS-based BOP Component Opportunities

Working with other HSECoE members, we have identified a number of additional applications for MECS including:

- Microchannel combustor/heat exchanger for solid and liquid chemical hydride systems
- Microchannel combustor heat exchanger to burn vented hydrogen from adsorbent tanks
- Cryogenic heat exchanger for adsorbent Systems
- Catalytic and absorption based MECS systems for ammonia removal from discharged hydrogen



Proposed FY 2010 Future Work

- Reduce Size and Weight of Storage and Improve Charging and Discharging Rates (Barriers A and E) - **MECS-based Tank Insert Development**
 - Complete simulation of optimized tank insert unit cell
 - Complete experimental validation of tank insert simulation and unit cell performance
 - Complete tank insert design including headers
 - Outline fabrication approach and production cost for numbering up tank insert
- Reduce size and weight and increase performance of thermal balance of plant components (Barrier H) - **MECS-based integrated combustor/heat exchanger/recuperator**
 - Complete simulation of optimized μ CHX
 - Complete μ CHX unit cell fabrication and testing
 - Experimentally validate μ CHX simulation
 - Demonstrate rapid start-up and transient performance of μ CHX



Collaboration

- Oregon State University is a member (a prime contractor) of the Hydrogen Storage Engineering Center of Excellence (HSECoE) which includes:
 - **Savannah River National Laboratory (Center Lead)**
 - **Pacific Northwest National Laboratory**
 - **Los Alamos National Laboratory**
 - **National Renewable Energy Laboratory**
 - **Jet Propulsion Laboratory**
 - **United Technologies Research Center**
 - **HSM Systems**
 - **Lincoln Composites**
 - **BASF**
 - **Universite' du Quebec a Trois-Rivieres**
 - **General Motors Company**
 - **Ford Motor Company**



Project Summary

- **Relevance:** Microchannel technology can reduce size, weight and charging time of hydrogen storage.
- **Approach:** For MECS-based tank insert and μ CHX
 - Use MECS techniques to enhance the performance of heat and mass transfer devices.
 - Optimize a single unit cell
 - Use microlamination to “Number Up” .
- **Technical Accomplishments:**
 - Completed identification of the highest value applications of microchannel-based technology (2009/2010 DOE milestone)
 - Completed design and fabrication of tank insert unit cell test apparatus
 - Completed design of μ CHX test apparatus and unit cell
- **Collaboration:** Member of HSECoE team.
- **Proposed Future Research:**
 - Complete simulation and testing of tank insert unit cell
 - Complete design and manufacturing cost estimate for tank insert
 - Complete design and testing of μ CHX



Supplemental Slides

What is MECS? - Applications

Fuel Processing

Chemical Processing

Heating & Cooling



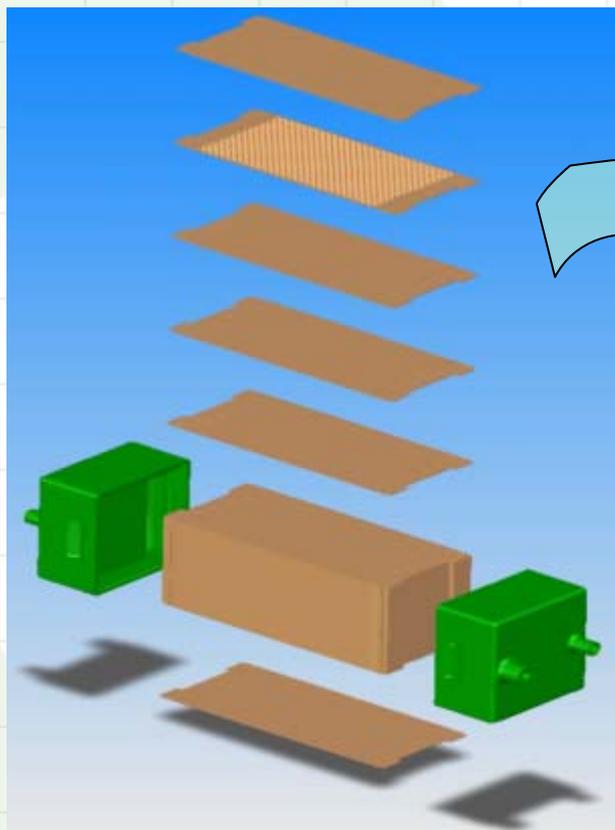
What is the Microproducts Breakthrough Institute (MBI)

- The MBI is a unique 40,000 sq ft product development laboratory operated by Oregon State University (OSU) and the Pacific Northwest National Laboratory (PNNL)
- The MBI is focused on the application of process intensification to energy and chemical systems miniaturization
- The MBI combines the expertise of the leading industrial (PNNL) and academic (OSU) research programs on process intensification and is a national leader in developing this technology
- The mission of the MBI is to develop and commercialize miniature energy and chemical systems

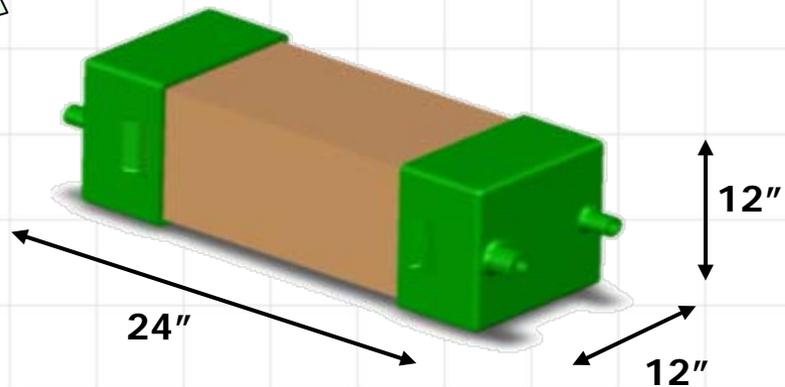
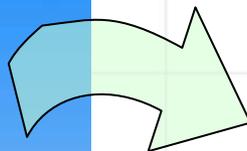


Microlamination

[Paul et al. 1999, Ehrfeld et al. 2000*]



Microlamination of Reactor



Microchannel Reactor

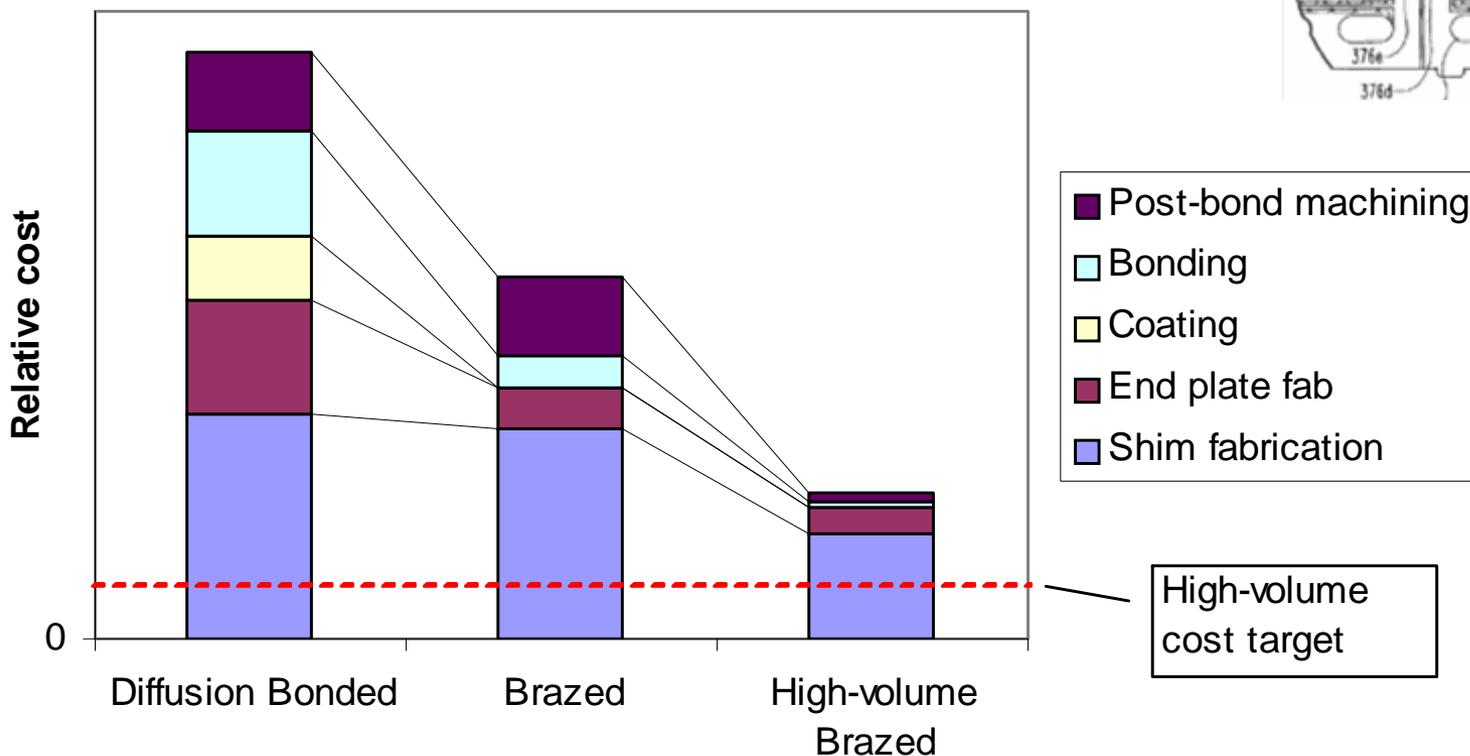
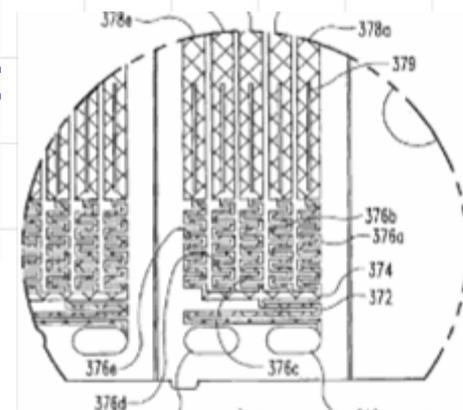
* W. Ehrfeld, V. Hessel, H. Löwe, Microreactors: New Technology for Modern Chemistry, Wiley-VCH, 2000.



Thermal Management Components

Al μ CHX Fabrication Costs

- Current industrial cost targets for Al microchannel components can be achieved by:
 - Scale-up of Al stamping
 - Developing and qualifying Al brazing processes



High-volume cost target

Al Microlamination

Microchannel Arrays (Eluri and Paul 2010)

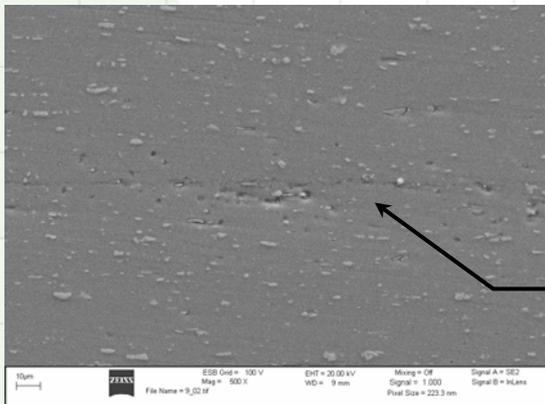
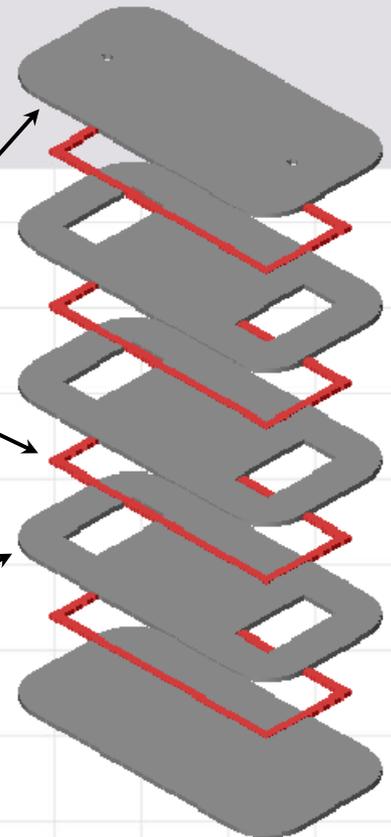


Microchannel Heat Exchanger

Interconnect

NP-Enhanced
Braze Paste

Plenum
Layer



- Precise Al brazing difficult due to oxides
- Seamless Al brazing demonstrated (550C)

Single-phase
Bondline

Microchannel
Array

